

NATIONAL EXAMINATIONS - December 2015

04-BS-10, Thermodynamics

3 Hours Duration

NOTES:

1. If doubt exists as to the interpretation of any question, the candidate is urged to submit, with the answer paper, a clear statement of any assumptions made.
 2. Any one of the approved calculator models is permitted. This is a "Closed-Book" examination with one 8.5×11 inch sheet of notes (both sides) allowed.
 3. Property tables and charts are provided where necessary.
 4. **Two** questions from part "A" plus **four** questions from part "B" (a total of **six** questions) constitutes a complete paper. Unless clearly indicated otherwise by you, only the first two questions from part "A" and the first four questions from part "B" that you answered will be marked.
 5. The mark associated with each question is specified.
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PART A. DO ONLY TWO OF QUESTIONS 1, 2, or 3(Each question is worth **20 marks**)

1. Water is the working fluid in a Rankine cycle. Superheated vapor enters the turbine at 8 MPa and 500°C. The condenser pressure is 10 kPa. The net power output of the cycle is 10⁵ kW. The turbine and pump have isentropic efficiencies of 85% and 70%, respectively. Let the environment conditions be $T_o=288$ K and $p_o=100$ kPa. Assume a source temperature of 1000 K and a sink temperature of 288 K. Show the cycle on a T-s diagram with respect to saturation lines. Determine
 - (a) the mass flow rate of steam in kg/s,
 - (b) the rate of heat transfer to the working fluid passing through the boiler in kW,
 - (c) the thermal efficiency of the cycle,
 - (d) the mass flow rate of condenser cooling water in kg/h, if the cooling water enters the condenser at 15°C and exits at 35°C with negligible pressure change,
 - (e) the second law efficiency of the cycle, and
 - (f) the exergy destruction associated with each of the processes in kJ/s.

2. Consider a regenerative gas turbine with a two-stage air compressor that operates at steady state, compressing 10 m³/min of air from 100 kPa and 300 K to 1 MPa. An intercooler between the two stages cools the air to 300 K at a constant pressure of 300 kPa. Each compressor stage has an isentropic efficiency of 85%. The turbine inlet temperature is 1300 K and the turbine has an isentropic efficiency of 87%. The regenerator effectiveness is 80%. Show the cycle on a T-s diagram. Accounting for the variation of specific heats with temperature, calculate
 - (a) the power required to run the compressor in kW,
 - (b) the thermal efficiency,
 - (c) the rate of heat addition in kW,
 - (d) the net power developed in kW,
 - (e) the rate of exergy destruction, in kJ/s, in each turbine and compressor stage if $T_o=300$ K, and
 - (f) the second law efficiency of the cycle assuming a source temperature of 1200 K and a sink temperature of 300 K.

3. Air enters the compressor of a gas refrigeration cycle at 100 kPa, 270 K. The compressor pressure ratio is 3 and the temperature at the turbine inlet is 310 K. The compressor and turbine have isentropic efficiencies of 85 and 88%, respectively. Assume variable specific heats for air. Show the cycle on a T-s diagram and determine
 - (a) the net work input, in kJ/kg,
 - (b) the heat removal from the refrigerated space, in kJ/kg,
 - (c) the coefficient of performance, and
 - (d) the entropy generation in the compressor and turbine, in kJ/kg K.

PART B. DO ONLY FOUR OF QUESTIONS 4, 5, 6, 7, 8 or 9(Each question is worth **15 marks**)

4. A mixture of 80% N₂, and 20% CO₂ gases (by mole numbers), is compressed isentropically in a compressor. The mixture enters the compressor at 100 kPa and 1000 K and leaves at 500 kPa. Assume constant specific heats at room temperature (300 K). Treat the mixture as an ideal gas. Determine the work input to the compressor per unit mass of the mixture.
5. The air in a room has a dry-bulb temperature of 25°C and a wet bulb temperature of 15°C. Assuming a pressure of 1 atm, determine
 - (a) the specific humidity,
 - (b) the relative humidity, and
 - (c) the dew-point temperature.
6. A rigid vessel with a volume of 0.05 m³ is initially filled with saturated water vapor at 100 kPa. Heat is now transferred from the water until the temperature reaches 75°C.
 - (a) Sketch the process on a P-v diagram with respect to the saturation lines.
 - (b) Find the final pressure.
 - (c) Find the heat transfer from the water.
7. Air enters a nozzle at 180 kPa and 707°C, with low velocity. The nozzle expands the air adiabatically to a pressure of 70 kPa. The isentropic efficiency of the nozzle is 90%. Sketch the process on a T-s diagram. Accounting for the variation of specific heats with temperature, determine
 - (a) the exit velocity of the air, and
 - (b) the exit temperature of the air.
8. 0.5 kg of air executes a Carnot power cycle having a thermal efficiency of 50%. The heat transfer to the air during the isothermal expansion is 40 kJ. At the beginning of the isothermal expansion, the pressure is 700 kPa and the volume is 0.12 m³. Determine
 - (a) the maximum and minimum temperatures for the cycle, in K,
 - (b) the volume at the end of the isothermal expansion, in m³, and
 - (c) the work and heat transfer for each of the four processes, in kJ.
9. A rigid tank of volume 0.5 m³ is initially evacuated. A tiny hole develops in the wall, and air from the surroundings at 100 kPa and 21°C leaks in. Eventually, the pressure in the tank reaches 100 kPa. The process occurs slowly enough that heat transfer between the tank and the surroundings keeps the temperature of the air inside the tank constant at 21°C. Determine the amount of heat transfer, in kJ.

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TABLE A-1
Molar mass, gas constant, and critical-point properties

Substance	Formula	Molar mass kg/kmol	R kJ/(kg · K)*	Temperature K	Pressure MPa	Volume m ³ /kmol
Ammonia	NH ₃	17.03	0.4882	405.5	11.28	0.0724
Argon	Ar	39.948	0.2081	151	4.86	0.0749
Bromine	Br ₂	159.808	0.0520	584	10.34	0.1355
Carbon dioxide	CO ₂	44.01	0.1889	304.2	7.39	0.0943
Carbon monoxide	CO	28.011	0.2968	133	3.50	0.0930
Chlorine	Cl ₂	70.906	0.1173	417	7.71	0.1242
Deuterium (normal)	D ₂	4.00	2.0785	38.4	1.66	—
Helium	He	4.003	2.0769	5.3	0.23	0.0578
Hydrogen (normal)	H ₂	2.016	4.1240	33.3	1.30	0.0649
Krypton	Kr	83.80	0.09921	209.4	5.50	0.0924
Neon	Ne	20.183	0.4119	44.5	2.73	0.0417
Nitrogen	N ₂	28.013	0.2968	126.2	3.39	0.0899
Nitrous oxide	N ₂ O	44.013	0.1889	309.7	7.27	0.0961
Oxygen	O ₂	31.999	0.2598	154.8	5.08	0.0780
Sulfur dioxide	SO ₂	64.063	0.1298	430.7	7.88	0.1217
Water	H ₂ O	18.015	0.4615	647.3	22.09	0.0568
Xenon	Xe	131.30	0.06332	289.8	5.88	0.1186
Benzene	C ₆ H ₆	78.115	0.1064	562	4.92	0.2603
<i>n</i> -Butane	C ₄ H ₁₀	58.124	0.1430	425.2	3.80	0.2547
Carbon tetrachloride	CCl ₄	153.82	0.05405	556.4	4.56	0.2759
Chloroform	CHCl ₃	119.38	0.06964	536.6	5.47	0.2403
Dichlorodifluoromethane (R-12)	CCl ₂ F ₂	120.91	0.06876	384.7	4.01	0.2179
Dichlorofluoromethane	CHCl ₂ F	102.92	0.08078	451.7	5.17	0.1973
Ethane	C ₂ H ₆	30.070	0.2765	305.5	4.88	0.1480
Ethyl alcohol	C ₂ H ₅ OH	46.07	0.1805	516	6.38	0.1673
Ethylene	C ₂ H ₄	28.054	0.2964	282.4	5.12	0.1242
<i>n</i> -Hexane	C ₆ H ₁₄	86.178	0.09647	507.9	3.03	0.3677
Methane	CH ₄	16.043	0.5182	191.1	4.64	0.0993
Methyl alcohol	CH ₃ OH	32.042	0.2595	513.2	7.95	0.1180
Methyl chloride	CH ₃ Cl	50.488	0.1647	416.3	6.68	0.1430
Propane	C ₃ H ₈	44.097	0.1885	370	4.26	0.1998
Propene	C ₃ H ₆	42.081	0.1976	365	4.62	0.1810
Propyne	C ₃ H ₄	40.065	0.2075	401	5.35	—
Trichlorofluoromethane	CCl ₃ F	137.37	0.06052	471.2	4.38	0.2478
Air	—	28.97	0.2870	—	—	—

*The unit kJ/(kg · K) is equivalent to kPa · m³/(kg · K). The gas constant is calculated from $R = R_u/M$, where $R_u = 8.314$ kJ/(kmol · K) and M is the molar mass.

Source: Gordon J. Van Wylen and Richard E. Sonntag, *Fundamentals of Classical Thermodynamics*, English/SI Version, 3d ed., Wiley, New York, 1986, p. 685, table A.6SI. Originally published in K. A. Kobe and R. E. Lynn, Jr., *Chemical Review*, vol. 52, pp. 117–236, 1953.

TABLE A-4

Saturated water—Temperature table

H₂O

Temp., T°C	Sat. press., P _{sat} kPa	Specific volume, m ³ /kg		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/(kg·K)		
		Sat. liquid, v _f	Sat. vapor, v _g	Sat. liquid, u _f	Evap., u _{fg}	Sat. vapor, u _g	Sat. liquid, h _f	Evap., h _{fg}	Sat. vapor, h _g	Sat. liquid, s _f	Evap., s _{fg}	Sat. vapor, s _g
0.01	0.6113	0.001000	206.14	0.0	2375.3	2375.3	0.01	2501.3	2501.4	0.000	9.1562	9.1562
5	0.8721	0.001000	147.12	20.97	2361.3	2382.3	20.98	2489.6	2510.6	0.0761	8.9496	9.0257
10	1.2276	0.001000	106.38	42.00	2347.2	2389.2	42.01	2477.7	2519.8	0.1510	8.7498	8.9008
15	1.7051	0.001001	77.93	62.99	2333.1	2396.1	62.99	2465.9	2528.9	0.2245	8.5569	8.7814
20	2.339	0.001002	57.79	83.95	2319.0	2402.9	83.96	2454.1	2538.1	0.2966	8.3706	8.6672
25	3.169	0.001003	43.36	104.88	2304.9	2409.8	104.89	2442.3	2547.2	0.3674	8.1905	8.5580
30	4.246	0.001004	32.89	125.78	2290.8	2416.6	125.79	2430.5	2556.3	0.4369	8.0164	8.4533
35	5.628	0.001006	25.22	146.67	2276.7	2423.4	146.68	2418.6	2565.3	0.5053	7.8478	8.3531
40	7.384	0.001008	19.52	167.56	2262.6	2430.1	167.57	2406.7	2574.3	0.5725	7.6845	8.2570
45	9.593	0.001010	15.26	188.44	2248.4	2436.8	188.45	2394.8	2583.2	0.6387	7.5261	8.1648
50	12.349	0.001012	12.03	209.32	2234.2	2443.5	209.33	2382.7	2592.1	0.7038	7.3725	8.0763
55	15.758	0.001015	9.568	230.21	2219.9	2450.1	230.23	2370.9	2600.9	0.7679	7.2234	7.9913
60	19.940	0.001017	7.671	251.11	2205.5	2456.6	251.13	2358.5	2609.6	0.8312	7.0784	7.9096
65	25.03	0.001020	6.197	272.02	2191.1	2463.1	272.06	2346.2	2618.3	0.8935	6.9375	7.8310
70	31.19	0.001023	5.042	292.95	2176.6	2469.6	292.98	2333.8	2626.8	0.9549	6.8004	7.7553
75	38.58	0.001026	4.131	313.90	2162.0	2475.9	313.93	2321.4	2635.3	1.0155	6.6669	7.6824
80	47.39	0.001029	3.407	334.86	2147.4	2482.2	334.91	2308.8	2643.7	1.0753	6.5369	7.6122
85	57.83	0.001033	2.828	355.84	2132.6	2488.4	355.90	2296.0	2651.9	1.1343	6.4102	7.5445
90	70.14	0.001036	2.361	376.85	2117.7	2494.5	376.92	2283.2	2660.1	1.1925	6.2866	7.4791
95	84.55	0.001040	1.982	397.88	2102.7	2500.6	397.96	2270.2	2668.1	1.2500	6.1659	7.4159
Sat. press., MPa												
100	0.10135	0.001044	1.6729	418.94	2087.6	2506.5	418.94	2257.0	2676.1	1.3069	6.0480	7.3549
105	0.12082	0.001048	1.4194	440.02	2072.3	2512.4	440.15	2243.7	2683.8	1.3630	5.9328	7.2958
110	0.14327	0.001052	1.2102	461.14	2057.0	2518.1	461.30	2230.2	2691.5	1.4185	5.8202	7.2387
115	0.16906	0.001056	1.0366	482.30	2041.4	2523.7	482.48	2216.5	2699.0	1.4734	5.7100	7.1833
120	0.19853	0.001060	0.8919	503.50	2025.8	2529.3	503.71	2202.6	2706.3	1.5276	5.6020	7.1296
125	0.2321	0.001065	0.7706	524.74	2009.9	2534.6	524.99	2188.5	2713.5	1.5813	5.4962	7.0775
130	0.2701	0.001070	0.6685	546.02	1993.9	2539.9	546.31	2174.2	2720.5	1.6344	5.3925	7.0269
135	0.3130	0.001075	0.5822	567.35	1977.7	2545.0	567.69	2159.6	2727.3	1.6870	5.2907	6.9777
140	0.3613	0.001080	0.5089	588.74	1961.3	2550.0	589.13	2144.7	2733.9	1.7391	5.1908	6.9299
145	0.4154	0.001085	0.4463	610.18	1944.7	2554.9	610.63	2129.6	2740.3	1.7907	5.0926	6.8833
150	0.4758	0.001091	0.3928	631.68	1927.9	2559.5	632.20	2114.3	2746.5	1.8418	4.9960	6.8379
155	0.5431	0.001096	0.3468	653.24	1910.8	2564.1	653.84	2098.6	2752.4	1.8925	4.9010	6.7935
160	0.6178	0.001102	0.3071	674.87	1893.5	2568.4	675.55	2082.6	2758.1	1.9427	4.8075	6.7502
165	0.7005	0.001108	0.2727	696.56	1876.0	2572.5	697.34	2066.2	2763.5	1.9925	4.7153	6.7078
170	0.7917	0.001114	0.2428	718.33	1858.1	2576.5	719.21	2049.5	2768.7	2.0419	4.6244	6.6663
175	0.8920	0.001121	0.2168	740.17	1840.0	2580.2	741.17	2032.4	2773.6	2.0909	4.5347	6.6256
180	1.0021	0.001127	0.19405	762.09	1821.6	2583.7	763.22	2015.0	2778.2	2.1396	4.4461	6.5857
185	1.1227	0.001134	0.17409	784.10	1802.9	2587.0	785.37	1997.1	2782.4	2.1879	4.3586	6.5465
190	1.2544	0.001141	0.15654	806.19	1783.8	2590.0	807.62	1978.8	2786.4	2.2359	4.2720	6.5079
195	1.3978	0.001149	0.14105	828.37	1764.4	2592.8	829.98	1960.0	2790.0	2.2835	4.1863	6.4698

TABLE A-4

Saturated water—Temperature table (Concluded)

Temp., T°C	Sat. press., P _{sat} MPa	Specific volume, m ³ /kg		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/(kg·K)		
		Sat. liquid, v _f	Sat. vapor, v _g	Sat. liquid, u _f	Evap., u _{fg}	Sat. vapor, u _g	Sat. liquid, h _f	Evap., h _{fg}	Sat. vapor, h _g	Sat. liquid, s _f	Evap., s _{fg}	Sat. vapor, s _g
200	1.5538	0.001157	0.13736	850.65	1744.7	2595.3	852.45	1940.7	2793.2	2.3309	4.1014	6.4323
205	1.7230	0.001164	0.11521	873.04	1724.5	2597.5	875.04	1921.0	2796.0	2.3780	4.0172	6.3952
210	1.9062	0.001173	0.10441	895.53	1703.9	2599.5	897.76	1900.7	2798.5	2.4248	3.9337	6.3585
215	2.104	0.001181	0.09479	918.14	1682.9	2601.1	920.62	1879.9	2800.5	2.4714	3.8507	6.3221
220	2.318	0.001190	0.08619	940.87	1661.5	2602.4	943.62	1858.5	2802.1	2.5178	3.7683	6.2861
225	2.548	0.001199	0.07849	963.73	1639.6	2603.3	966.78	1836.5	2803.3	2.5639	3.6863	6.2503
230	2.795	0.001209	0.07158	986.74	1617.2	2603.9	990.12	1813.8	2804.0	2.6099	3.6047	6.2146
235	3.060	0.001219	0.06537	1009.89	1594.2	2604.1	1013.62	1790.5	2804.2	2.6558	3.5233	6.1791
240	3.344	0.001229	0.05976	1033.21	1570.8	2604.0	1037.32	1766.5	2803.8	2.7015	3.4422	6.1437
245	3.648	0.001240	0.05471	1056.71	1546.7	2603.4	1061.23	1741.7	2803.0	2.7472	3.3612	6.1083
250	3.973	0.001251	0.05013	1080.39	1522.0	2602.4	1085.36	1716.2	2801.5	2.7927	3.2802	6.0730
255	4.319	0.001263	0.04598	1104.28	1596.7	2600.9	1109.73	1689.8	2799.5	2.8383	3.1992	6.0375
260	4.688	0.001276	0.04221	1128.39	1470.6	2599.0	1134.37	1662.5	2796.9	2.8838	3.1181	6.0019
265	5.081	0.001289	0.03877	1152.74	1443.9	2596.6	1159.28	1634.4	2793.6	2.9294	3.0368	5.9662
270	5.499	0.001302	0.03564	1177.36	1416.3	2593.7	1184.51	1605.2	2789.7	2.9751	2.9551	5.9301
275	5.942	0.001317	0.03279	1202.25	1387.9	2590.2	1210.07	1574.9	2785.0	3.0208	2.8730	5.8938
280	6.412	0.001332	0.03017	1227.46	1358.7	2586.1	1235.99	1543.6	2779.6	3.0668	2.7903	5.8571
285	6.909	0.001348	0.02777	1253.00	1328.4	2581.4	1262.31	1511.0	2773.3	3.1130	2.7070	5.8199
290	7.436	0.001366	0.02557	1278.92	1297.1	2576.0	1289.07	1477.1	2766.2	3.1594	2.6227	5.7821
295	7.993	0.001384	0.02354	1305.2	1264.7	2569.9	1316.3	1441.8	2758.1	3.2062	2.5375	5.7437
300	8.581	0.001404	0.02167	1332.0	1231.0	2563.0	1344.0	1404.9	2749.0	3.2534	2.4511	5.7045
305	9.202	0.001425	0.019948	1359.3	1195.9	2555.2	1372.4	1366.4	2738.7	3.3010	2.3633	5.6643
310	9.856	0.001447	0.018350	1387.1	1159.4	2546.4	1401.3	1326.0	2727.3	3.3493	2.2737	5.6230
315	10.547	0.001472	0.016867	1415.5	1121.1	2536.6	1431.0	1283.5	2714.5	3.3982	2.1821	5.5804
320	11.274	0.001499	0.015488	1444.6	1080.9	2525.5	1461.5	1238.6	2700.1	3.4480	2.0882	5.5362
330	12.845	0.001561	0.012996	1505.3	993.7	2498.9	1525.3	1140.6	2665.9	3.5507	1.8909	5.4417
340	14.586	0.001638	0.010797	1570.3	894.3	2464.6	1594.2	1027.9	2622.0	3.6594	1.6763	5.3357
350	16.513	0.001740	0.008813	1641.9	776.6	2418.4	1670.6	893.4	2563.9	3.7777	1.4335	5.2112
360	18.651	0.001893	0.006945	1725.2	626.3	2351.5	1760.5	720.3	2481.0	3.9147	1.1379	5.0526
370	21.03	0.002213	0.004925	1844.0	384.5	2228.5	1890.5	441.6	2332.1	4.1106	0.6865	4.7971
374.14	22.09	0.003155	0.003155	2029.6	0	2029.6	2099.3	0	2099.3	4.4298	0	4.4298

Source: Tables A-4 through A-8 are adapted from Gordon J. Van Wylen and Richard E. Sonntag, *Fundamentals of Classical Thermodynamics*, English/SI Version, 3rd ed. (New York: John Wiley & Sons, 1986), pp. 635–651. Originally published in Joseph H. Keenan, Frederick G. Keyes, Philip G. Hill, and Joan G. Moore, *Steam Tables*, SI Units (New York: John Wiley & Sons, 1978).