# NATIONAL EXAMINATIONS - December 2018 

04-BS-10, Thermodynamics

## 3 Hours Duration

## NOTES:

1. If doubt exists as to the interpretation of any question, the candidate is urged to submit, with the answer paper, a clear statement of any assumptions made.
2. Any one of the approved Casio or Sharp calculator models is permitted. This is a "Closed-Book" examination with one $8.5 \times 11$ inch sheet of notes (both sides) allowed.
3. Property tables and charts are provided where necessary. Interpolation is not necessary. The closest tabular value may be used.
4. Two questions from part " $A$ " plus four questions from part " $B$ " (a total of six questions) constitutes a complete paper. Unless clearly indicated otherwise by you, only the first two questions from part " $A$ " and the first four questions from part "B" that you answered will be marked.
5. The mark associated with each question is specified.

## PART A. DO ONLY TWO OF QUESTIONS 1, 2, or 3

(Each question is worth 20 marks)

1. Consider a regenerative vapor power cycle with two feedwater heaters, a closed one and an open one, as shown in the figure. Steam enters the first turbine stage at $12 \mathrm{MPa}, 480^{\circ} \mathrm{C}$, and expands to 2 MPa . Some steam is extracted at 2 MPa and fed to the closed feedwater heater. The remainder expands through the secondstage turbine to 0.3 MPa , where an additional amount is extracted and fed into the open feedwater heater operating at 0.3 MPa . The steam expanding through the third-stage turbine exits at the condenser pressure of 6 kPa . Feedwater leaves the closed heater at $210^{\circ} \mathrm{C}, 12 \mathrm{MPa}$, and condensate exiting as saturated liquid at 2 MPa is trapped into the open feedwater heater. Saturated liquid at 0.3 MPa leaves the open feedwater heater. Assume all pumps and turbine stages operate isentropically. Show the cycle on a T-s diagram with respect to saturation lines, and determine
(a) the rate of heat transfer to the working fluid passing through the steam generator, in kJ per kg of steam entering the first-stage turbine,
(b) the net power output, in kJ per kg of steam entering the first-stage turbine,
(c) the thermal efficiency of the cycle, and
(d) the second law efficiency of the cycle assuming a source temperature of 1000 K and a sink temperature of 288 K .

2. Air enters the compressor of a cold air-standard Brayton cycle with regeneration at $100 \mathrm{kPa}, 300 \mathrm{~K}$, with a mass flow rate of $6 \mathrm{~kg} / \mathrm{s}$. The compressor pressure ratio is 10 , and the turbine inlet temperature is 1400 K . The turbine and compressor each have isentropic efficiencies of $80 \%$ and the regenerator effectiveness is $80 \%$. Sketch the cycle on a T-s diagram. For $k=1.4$, determine
(a) the thermal efficiency of the cycle,
(b) the back work ratio,
(c) the net power developed, in kW ,
(d) the rate of exergy destruction in the regenerator, turbine and compressor, in kW , for $\mathrm{T}_{0}=300 \mathrm{~K}$.
3. A vapor-compression refrigeration system with two evaporators using Refrigerant 134a as the working fluid is shown in the figure. The low-temperature evaporator operates at $-18^{\circ} \mathrm{C}$ with saturated vapor at its exit and has a refrigerating capacity of 3 tons. The higher-temperature evaporator produces saturated vapor at 320 kPa at its exit and has a refrigerating capacity of 2 tons. The compressor has an isentropic efficiency of $90 \%$ and the condenser pressure is 1 MPa . There are no significant pressure drops in the flow through the condenser and the two evaporators. The refrigerant leaves the condenser as saturated liquid at 1 MPa . Show the cycle on a T-s diagram with respect to saturation lines. Determine
(a) the mass flow rate of refrigerant through each evaporator, in $\mathrm{kg} / \mathrm{min}$
(b) the compressor power input, in kW ,
(c) the coefficient of performance (COP) of the cycle,
(d) the entropy increase in the compressor, in kW/K.
( 1 ton $=211 \mathrm{~kJ} / \mathrm{min}$ )


PART B. DO ONLY FOUR OF QUESTIONS 4, 5, 6, 7, 8 or 9
(Each question is worth 15 marks)
4. A mixture with a mass of 2 kg having a mass fraction of $70 \% \mathrm{~N}_{2}$ and $30 \% \mathrm{O}_{2}$ is compressed adiabatically from 100 kPa and $7^{\circ} \mathrm{C}$ to 500 kPa and $177^{\circ} \mathrm{C}$, Determine
a. the work input in kJ , and
b. the amount of entropy produced in $\mathrm{kJ} / \mathrm{K}$
5. Moist air at $25^{\circ} \mathrm{C}, 105 \mathrm{kPa}, 85 \%$ relative humidity and a volumetric flow rate of $0.3 \mathrm{~m}^{3} / \mathrm{s}$ enters a well-insulated compressor operating at steady state. If moist air exits at $97^{\circ} \mathrm{C}$ and 200 kPa , determine
(a) the relative humidity at the compressor exit, and
(b) the power input to the compressor in kW .

Hint: $\omega$ inlet $=\omega$ exit
6. Air is contained in a rigid well-insulated tank with a volume of $0.2 \mathrm{~m}^{3}$. The tank is fitted with a paddle wheel that transfers energy to the air at a constant rate of 4 W for 20 min . The initial density of the air is $1.2 \mathrm{~kg} / \mathrm{m}^{3}$. If no changes in kinetic or potential energy occur, determine
(a) the specific volume at the final state, in $\mathrm{m}^{3} / \mathrm{kg}$,
(b) the change in specific internal energy of the air, in $\mathrm{kJ} / \mathrm{kg}$.
7. A piston-cylinder assembly contains 5 kg of two-phase liquid-vapor mixture of $\mathrm{H}_{2} \mathrm{O}$ initially at 500 kPa with a quality of $98 \%$. Expansion occurs to a state where the pressure is 150 kPa . During the process the pressure and specific volume are related by $p v=$ constant. Determine
(a) the work, in kJ , and
(b) the heat transfer, in kJ .
8. Air expands at a mass flow rate of $10 \mathrm{~kg} / \mathrm{s}$ through a turbine from $500 \mathrm{kPa}, 900 \mathrm{~K}$ to $100 \mathrm{kPa}, 600 \mathrm{~K}$. The inlet velocity is small compared to the exit velocity of 100 $\mathrm{m} / \mathrm{s}$. The turbine operates at steady state. Heat transfer from the turbine to the surroundings and potential energy effects are negligible. Calculate
(a) the power developed by the turbine, in kW , and
(b) the turbine exit area, in $\mathrm{m}^{2}$.
9. $\quad 1.5 \mathrm{~kg}$ of air (Assume ideal gas behavior) executes a Carnot power cycle having a thermal efficiency of $50 \%$. The heat transfer to the air during the isothermal expansion is 40 kJ . At the beginning of the isothermal expansion, the pressure is 700 kPa and the volume is $0.12 \mathrm{~m}^{3}$. Sketch the cycle on $p-v$ diagram and determine
(a) the maximum and minimum temperatures for the cycle, in K ,
(b) the volume at the end of the isothermal expansion, in $\mathrm{m}^{3}$, and
(c) the work and heat transfer for each of the four processes, in kJ .

## APPENDIX - TABLES AND CHART

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TABLE A. 1

|  | a | Molar mass $\mathrm{kg} / \mathrm{kmol}$ | $\begin{aligned} & R \\ & \mathrm{~kJ} /(\mathrm{kg} \cdot \mathrm{~K})^{*} \end{aligned}$ | Temperature K | Pressure MPa | Valume $\mathrm{mi}^{3} / \mathrm{kmal}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Substance | Forma | 17.03 | 0.4882 | 405.5 | 11.28 | 0.0724 |
| Ammonia | $\mathrm{NH}_{3}$ | 17.03 | 0.2081 | 151 | 4.86 | 0.0749 |
| Argon | Ar | 39.948 | 0.0520 | 584 | 10.34 | 0.1355 |
| Bromine | $\mathrm{Br}_{2}$ | 159.808 | 0.0520 | 304.2 | 7.39 | 0.0943 |
| Carbon dioxide | $\mathrm{CO}_{2}$ | 44.01 | 0.1889 0.2968 | 133 | 3.50 | 0.0930 |
| Carbon monoxide | CO | 28.011 | 0.1173 | -417 | 7.71 | 0.1242 |
| Chlorine | $\mathrm{Cl}_{2}$ | 70.906 | 20785 | 38.4 | 1.66 | - |
| Deuterium (normal) | $\mathrm{D}_{2}$ | 4.00 | 2.0785 | 5.3 | 0.23 | 0.0578 |
| Helium | He | 4.003 | 4.0769 | 33.3 | 1.30 | 0.0649 |
| Hydragen (normal) | $\mathrm{H}_{2}$ | 2.016 | 0.09921 | 209.4 | 5.50 | 0.0924 |
| Kryplon | Kr | 83.80 | 0.4119 | 44.5 | 2.73 | 0.0417 |
| Neon | Ne | 20.183 | 0.2968 . | 126.2 | 3.39 | 0.0859 |
| Nilrogen | $\mathrm{N}_{2}$ | 28.013 | 0.1889 | 309.7 | 7.27 | 0.0961 |
| Nitrous oxide | $\mathrm{N}_{2} \mathrm{O}$ | 44.013 | 0.1889 0.2598 | 154.8 | 5.08 | 0.0780 |
| Oxygen | $\mathrm{O}_{2}$ | 31.999 | 0.1298 | 430.7 | 7.88 | 0.1217 |
| Sulfur dioxide | $\mathrm{SO}_{2}$ | 64.063 18.015 | 0.4615 | 647.3 | 22.09 | 0.0568 |
| Water | $\mathrm{H}_{2} \mathrm{O}$ | 18.015 | 0.06332 | 289.8 | 5.88 | 0.1186 |
| Xenon | Xe | 131.30 | 0.1064 | 562 | 4.92 | 0.2603 |
| Benzene | $\mathrm{C}_{6} \mathrm{H}_{\mathrm{a}}$ | 78.115 | 0.1430 | 425.2 | 3.80 | 0.2547 |
| $n$-Butane | $\mathrm{Ca}_{4} \mathrm{H}_{10}$ - | 58.124 | 0.05405 | 556.4 | 4.56 | 0.2759 |
| Carbon letrachlorlde | $\mathrm{CCl}_{4}$ | 153.82 119.38 | 0.05405 | 536.6 | 5.47 | 0.2403 |
| Chlorolorm | $\mathrm{CHCl}_{3}$ | 119.38 | 0.06876 | 384.7 | 4.01 | 0.2179 |
| Dichlorodifluoromethane (R-12) | $\mathrm{CCl}_{2} \mathrm{~F}_{2}$ | 120.91 102.92 | 0.08078 | 451.7 | 5.17 | 0.1973 |
| Dichlorolluoromethane | $\mathrm{CHCl}_{2} \mathrm{~F}$ | 102.92 30.070 | 0.2765 | 305.5 | 4.88 | 0.1480 |
| Ethane | $\mathrm{C}_{2} \mathrm{H}_{5}$ | 30.070 | 0.1805 | 516 | 6.38 | 0.1673 |
| Elhyl alcotiol | $\mathrm{C}_{2} \mathrm{H}_{5} \mathrm{OH}$ | 46.07 28.054 | 0.2964 | 282.4 | 5.12 | 0.1242 |
| Elhyleñe | $\mathrm{C}_{2} \mathrm{H}_{4}$ | 28.054 86.178 | 0.09647 | 507.9 | 3.03 | 0.3677 |
| n-Hexane | $\mathrm{C}_{6} \mathrm{H}_{14}$ | 86.178 | 0.5182 | 191.1 | 4.64 | 0.0993 |
| Methane | $\mathrm{CH}_{4}$. | 16.043 32.042 | 0.51895 | 513.2 | 7.95 | 0.1180 |
| Methyl alcohol | $\mathrm{CH}_{3} \mathrm{OH}$ | 32.042 | 0.1647 | 416.3 | 6.68 | 0.1430 |
| Methyl chloride | $\mathrm{CH}_{3} \mathrm{Cl}$ | 50.488 | 0.1885 | 370 | 4.26 | 0.1998 |
| Propane | $\mathrm{C}_{3} \mathrm{H}_{8}$ | 44.097 | 0.1976 | 365 | 4.62 | 0.1810 |
| Propene | $\mathrm{C}_{3} \mathrm{H}_{6}$ | 065 | 0.2075 | 401 | 5.35 | :- |
| Propyne | $\mathrm{C}_{3} \mathrm{H}_{4}$ | ${ }_{137} 40.065$ | 0.06052 | 471.2 | 4.38 | 0.2478 |
| Trichloroflucromelhane | $\mathrm{CCl}_{3} \mathrm{~F}$ | 137.37 | 0.06870 | -: | - | - |
| Alr | - | 28.97 | 0.2870 | - |  |  |

The unil $\mathrm{kJ} /(\mathrm{kg} \cdot \mathrm{K})$ is equivalent to $\mathrm{kPa} \cdot \mathrm{m}^{3} /(\mathrm{kg} \cdot \mathrm{K})$. The gas conslant is calculated from $R=R_{u} / \mathrm{M}$, where $R_{u}=8.314 \mathrm{~kJ} /(\mathrm{kmol} \cdot \mathrm{k})$ and $M$ is the molar mass.
Sourca-Gordon J. Van Wylen and Richard E. Sonntag. Fundamentals of Classical Themodynamics, English/Si Verslon, 3d ed., Wley,
 Now
1953.


TABLE A-4


Sounco: Tables A-4 through A-8 are adapted from Gordon J. Van Wylen and Richard E. Sorintag. Findamantals of Classical Thermiodynimilces, Englist/Si. Verslon, 3rd ed. (New York: Jotin Wiley \& Sons, Is Units (New York: Johin. Wiay \& Sonis, 1978).
Keenan, Frederlck G. Koyos, Phillp G. Hill, and Joan G. Mooro, Sleam Tables, St Units' (New

TABLEA.5

| Saturated water-Pressure table |  |  |  | Internal energy, $\mathrm{kJ} / \mathrm{kg}$ |  |  | Enthalpy, $\mathrm{kJ} / \mathrm{kg}$ |  |  | $\begin{aligned} & \text { Entropy, } \\ & \mathrm{k} J /(\mathrm{kg} \cdot \mathrm{~K}) \end{aligned}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| \% |  |  |  |  |  |  |  |  |  |  |  | sat. |
| -20 ${ }^{0}$ | Sat. tomp. | Sat. liquid, | Sat. vapor, | Sat. | Evap.4 | vapor, | Sat. <br> liquid, $h_{1}$ | Evap. 1 In | sxpor, <br> \% | Sat. <br> IIquid, $s$, | Evap.ı $s_{0}$ | $s_{j}$ |
| SE: PKPX | $T_{s a t}{ }^{\text {c }}$ - | $v_{1}$ | $\boldsymbol{r}_{6}$. | tlquid, $u_{1}$ | $U_{4}$ | $u_{0}$ |  | $\frac{140}{2501.3}$ | 2501.4 | 0.0000 | 9.1562 | 9.1662 |
| -8is 0.6113 | 0.01 | 0,001000 | 206.14 | . 0.00 | 2375.3 | 2375.3 |  | 2484.9 | 2514.2 | 0.1059 | 8.8697 | 8.9758 |
| 1.0 | 6.98 | 0.001000 | 128.21* | 29.30 | 2355.7 | 2393.3 | 54.71 | 2470.6 | 2525.3 | 0.1957 | 8.6322 | 6.8279 |
| 1.5 | 13.03 | 0.001001 | 87.98 |  |  | 2399.5 | 73.48 | 2460.0 | 2533.5 | 0.2607 | 8.4629 | . 62437 |
| 2.0 | 17.50 | 0.001001 | 67.00 | 73.48 |  | 2404.4 | 88.49 | 2451.6 | 2540.0 | 0.3120 | 8.3311 | . 6436 |
| 2.5 | 21.08 | 0.001002 | 54.25 | 88.48 | 7.5 | 2408.5 | 101.05 | 2444.5 | 2545.5 | 0.3545 | 8.2231 | 8. 4746 |
| 3.0 | 24.08 | 0.001003 | 45.67 | 101.04 | 93.7 | 2415.2 | 121.46 | 2432.9 | 2554.4 | 0.4226 | 8.0520 | . 3951 |
| 4.0 | 28.86 | 0.001004 | 34.80 | 121.45 | 27 | 2420.5 | 137.82 | 2423.7 | 2561.5. | 0.4764 | 7.9187 | 2515 |
| 5.0 | 32.06 | 0.001005 | 28.19 | 13 | 1.7 | 2430.5 | 168.79 | 2406.0 | 2574.8 | 0.6764 | 7.6750 | 2 |
| 7.5 | 40,29 | 0.001008 | 9.24 | 8,78 | 6.1 | 2437.9 | 191.83 | 2392B | 2584,7 | 0.453 | ? | 5 |
| 10 | 45.81 | 0.001010 | 14.67 | 191.8 | 28 | 2448.7 | 225.94 | 2373.1 | 2599.1 | 0.7549 | 7.2536 | . 80005 |
| 15 | 53.97 | 0.001014 | 10 | 225.92 | 5.4 | 2456.7 | 251.40 | 2358.3 | 2609.7 | 0.8320 | 7.0766 | 7.8314 |
| 20 | 60.06 | 0.001017 | 7.649 | 2 | 2191.2 | 2463.1 | 271.93 | 2346.3 | 2618.2 | 0.8931 | 6.9363 | 7.7686 |
| 25 | 64.97 | 0.001020 | 6.204 |  | 2179.2 | 2468.4 | 289.23 | 2336.1 | 2625.3 | 0.8479 | 1 | 7.6700 |
| 30 | 69.10 | 0.00 | 5.229 |  | 2159.5 | 2477.0 | 317.58 | 2319.2 | 2636.8 | 1.0259 |  | 7.6939 |
| 40 | 75.87 | 0.0010 | 3.993 |  | 2143.4 | 2483.9 | 340.49 | 2305.4 | 2645.9 | 1.09130 | 6.2434 | 7.4584 |
| 50 | 81.33 | 0.001030 | 2217 | 384.31 | 2112.4 | 2496.7 | 384.39 | 2278.6 | 2663.0 | 1.2130 |  |  |
| 75 | 91.78 | 0.001037 | 2217 |  |  |  |  |  |  |  |  |  |
| Pross.y |  |  |  |  |  |  |  |  |  | 1.3026 | 6,0568 | 1:2594 |
| MPA . | * |  |  | 417.36 | 2088.7 | 2506.1 | 417.46 | 2258.0 | 2685.4 | 1.3740 | 5.9104 | 7.2844 |
| 0.100. | 89.63 | 0,001043 0.001048 | 1.6940 | 444.19 | 2069.3 | 2513.5 | 444.32 467.11 | 2241.0 | 2685.4 | 1.3743 1.4336 | 6.7897 | 72013 |
| 0.125 | 105.99 11.4 | 0.001048 0.001053 | 1.3749 1.1593 | 466.94 | 20527 | 2510.7 | 467.11 | 2226.6 | 2700.6 | 1.4849 | 6,6868 | 7.1717 |
| 0.150 | 114.37 | 0.001053 0.001057 | 1.1 .0036 | 486.80 | 2038.1 | 2524.9 | 488.99 | 2213.6 | 2706.7 | 1.5301 | 5.5970 | 7.1271 |
| 0.175 | 118.06 | 0.001057 0.001061 | 0.8857 | 504.49 | 2025.0 | 2529.6 | 60A.70 | 2201.8 |  | 1.6706 | 5.5173 | 7.0078 |
| 0.200 | 120:23 | 0.001061 0.001084 | 0.8857 0.7833 | 620.47 | 2013.1 | 2533.6 | 520.72 | 2181.3 | 2716.8 | 1.6072 | 5.4455 | 7.0527 |
| 0.225 | - 124500 | 0.001064 | 0.7187 | 535.10 | 20021 | 2537.2 | 635.37 | 2181.5 | 2721.3 | 1.6408 | 6.3801 | -7.0209 |
| 0.250 | 127.44 | 0.001067 0.001070 | 0.6573 | 64E.59 | 1901.8 | 2540.5 | 648.89 | 21724 |  | . 1.6716 | 5.3201 | 6.9919 |
| 0.275 | 130.60 | 0.001070 | 0.6573 | 561.15 | -1982.4 | 2543.6 | 561.47 | 2163.8 | 2725.3 | 1.7006 | 5.2646 | 6.9652 |
| 0.300 | . 133.65 | . 0.001073 | 0.6058 | 672.90 | 1973.6 | 2546.4 | 673.25 | 2155.8 | . 0 | 1.7006 | 5.2130 | 6.9405 |
| 0.325 | 136.30 | 0.001076 | 0.5620 0.5243 | 683.95 | 1965.0 | 2548.9 | 581.33 | 2158.1. | 2732.4 | 1.7528 | 6.4647 | 6.9176 |
| 0.250 | 138.88 | 0.001079 | 0.5243 | 694.40 | 1956.9 | 2551.3 | E94:81 | 2140.8 | 2735.6 | 1.7766 | 5.1193 | 6,8959 |
| 0.375 | 141.32 | 0.001081. | 0.4914 | 604.31 | 1949.3 | 2553.6 | 604.74 | 2133.8 | 2738.6 | 1.8207 | 5.0359 | 6.8565 . |
| 0.40 | 143.63 | 0.001084 | 0.4625 0.4140 | 622.77 | 1934.9 | 2557.6 | 623.26 | 2120.7 | 2743.9 | 1.8607 | 4.0606 | 6.8213 |
| 0.45 | 147.03 | 0.001088 | 0.4140 | 639.68 | 1821.6 | 2561.2 | 640.23 | 2108.5 | 2748.7 | 1.8607 | 4.8920 | 6.7693 |
| 0.50 | 151.86 | 0.001093 | - 0.3749 | 655.32 | 1809.2 | 2564.5 | 665.93 | 2097.0 | 2753.0 | 1.8973 | 4.8288 | 6.7600 |
| 0.65 | 155.48 | 0.001097 | 0.3427 | 669.80 | 1897.5 | 2567.4 | 670.50 | 2086.3 | 2756.8 | 1.8312 | 4.7703 | 6.7331 |
| 0.60 | 158.85 | 0.001101 | 0. | 683.66 | 1886.5 | 2570.1 | 684.28 | 2076.0 | 2760.3 | 1.89822 | 4.7158 | 6.7000 |
| 0.65 | 16201 | 0.001104 | 0.2 | 696.44 | 1876.1 | 2572.5 | 697.22 | 2066.3 | 2763.5 | 1.8922 | 4.6647 | 6.6847 |
| 0.70 | 164.87 | 0,001.108 | 0.2729 | 708.64 | 1866.1 | 2574.7 | 709.47 | 2057.0 | 2766.4 | 2.0462 | 4.6168 | 0.6630 |
| 0.75 | 167.78 | 0.001112 |  | 720.22 | 1856.6 | 2576.6 | 721.11 | 2048.0 | 2769.1 | 2.0710 | 4.6711 | 6.6421 |
| 0.60 | 170.43 | 0.001116 | 0.2 | 731.27 | 1847.4 | 2578.7 | 732.22 | 2039.4 | 2771.6 | 2.0946 | 4.5280 | 6.6226 |
| 0.85 | 172.86 | 0.001118 |  | 741.83 | 1838.6 | 2580.5 | 742.83 | 2031.1 |  | 2.1172 | 4.4669 | 6.6041 |
| 0.90 | 175.36 | 0.001121 | 0.2150 |  | 1830.2 | 25821 | 753.02 | 2023.1 | 2776.1 |  | 4.4478 | 6.5865 |
| 0.95 | 177.69 | 0.001124 | 0.2402 | 761.68 | 1822.0 | 2583.6 | 76281 | 2015.3 | 2778.1 | 2.387 | 4.3744 | $6.5536{ }_{1}$ |
| 1.00 | 178.91 | 0.001127 | 0.19444 | 780.09 | 1806.3 | 2586.4 | 781.34 | 2000.4 | 2871.7 | 2 | 4.3067 | 6.5233. |
| 1.10 | 184.09 | 0.001133 | 0.17763 | 780.09 | 1791.5 | 2588.8 | 788.65 | 1986.2 | 2784.8 | 22160 | 4.2438 | $6.4853^{\circ}$ |
| 1.20 | 187.99 | 0.001139 | 0.16333 |  | 1777.5 | 2591.0 | B14.83 | 1972.7 | 2787.6 | 22515 |  |  |

TABLEA-5

| $\frac{\text { Saturated water-Pressure table (Concl }}{\text { Specific volume, }}$ |  |  |  | Internal energy, $\mathrm{kJ} / \mathrm{kg}$ |  |  | Entitialipy,$\mathrm{k} J / \mathrm{kg}$ |  |  | $\begin{aligned} & \text { Entropy, } \\ & \mathrm{kd} /(\mathrm{kg} \cdot \mathrm{~K}) \end{aligned}$ |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Pressas PMPa | Sat. <br> temp., $T_{\text {sat }}{ }^{\circ} \mathrm{C}$ | Sat. liquid, $v_{1}$ | Sat. <br> vapor, $v_{j}$ | Sat. liquid, $u_{f}$ | Evap.s $U_{p}^{\prime}$. | Sat. vapor, $u_{p}$ | Sat. <br> liquid, <br> $h_{f}$ | Euap., $h_{\text {lq }}$ | Sat. vapor $h_{0}$ | Sat. Ilquid, $s_{f}$ | Evap., <br> $s_{10}$ <br> 41850 | Sat. <br> vapor, <br> $s_{0}$ |  |
|  | 195.07 | 0.001149 | 0.14084 | 828.70 | 1764.1 | 2592.8 | 830.30 | 1957.7 | 2790.0 | 2.2842 | 4.1850 | 6.4448 |  |
| 1.50 | 198.32 | 0.001154 | 0.13177 | 843.16 | 1751.3 | 2594.5 | 844.89 | 1947.3 | 2792.2 | 23150 | 4.1298 4.0044 | 6.4448 6.3896 |  |
| 1.75 | 205.76 | 0.001166 | 0.11349 | 876.46 | 1721.4 | 259 | 878.50 | 18 | 2799.5 | 24474 | 3.8935 | 6,3409 |  |
| 2.00 | 212.42 | 0.001177 | 0.09963 | 906.44 | 1693.8 | 2600 | 936.49 | 1865 | 2801.7 | 2.5035 | 3.7937 | 6.2972 |  |
| 2.25 | 218.45 | 0.001.187 | 0.08875 | 933.83 | 1668.2 | 2603 | 962.11 | 1841.0 | 2803.1 | 2.5547 | 3.7028 | 6.2575 |  |
| 2.5 | 223.99 | 0.001197 | 0.07998 | 959.11 | 1644.0 | 2604.1 | 1008.42 | 1795.7 | 2804.2 | 2.6457 | 3.5412 | 6.1869 |  |
| 3.0 | 233.90 | 0.001217 | 0.06668 | 1004.78 |  | 2603.7 | 1049.75 | 1753.7 | 2803.4 | 2.7253 | 3.4000 | 6.1253 |  |
| 3.5 | 242.60 | 0.001235 | 0.05707 | 1045.43 |  | 2602.3 | 1087.3i | 1744.1 | 2801.4 | 27.664 | 3.2737 | 6.0701 |  |
| 4 | 250.40 | 0.001252 | 0.04978 | 1082.31 |  | 2597.1 | 1154.23 | 1640.1 | 2794.3 | 2.9202 | 3.0532 | 5.9734 |  |
| 5 | 263.99 | 0.001286 | 0.03944 | 1147.81 |  | 2589.7 | 1213.35 | 1571.0 | 2784.3 | 3.0267 | 2.8625 | 5.8892 |  |
| 6 | 275.64 | 0.001319 | 0.03244 | 1205 |  | 2580.5 | 1267.00 | 1505.1 | 27721 | 3.1211 | 2.6922 | 5.8133 |  |
| 7 | 285.88 | 0.001351 | 0.02737 | 1257.55 | 1323.0 | 2569.8 | 1316.64 | 1441.3 | 2758.0 | 3.2068 | 2.5364 | 5.7432 |  |
| 8 | 295.06 | 0.001384 | 0.02352 | 1305.57 | 1 | 2557.8 | 1363.26 | 1378.9 | 2742.1 | 3.2858 | 23915 | 5.6722 |  |
| 9 | 303.40 | 0.001418 | 0.02048 | 1350.51 | 1151.4 | 2544.4 | 1407.56 | 1317.1 | 2724.7 | 3.3596 | 2.2544 | 5.6141 |  |
| 10 | 311.06 | 0.001452 | 0.01802 |  | 1096.0 | 2529.8 | 1450.1 | 1255.5 | 2705.6 | 3.4295 | 21293 | 5.5527 |  |
| 11 | 318.15 | 0.001489 | 0.015987 | 1439.7 | 1040.7 | 2513.7 | 1491.3 | 1193.3 | 2684.9 | 3.4962 | 1.9962 | 5.4924 |  |
| 12 | 324.75 | 0.001527 | 0.014263 | 1473.0 | 985.0 | 2496.1 | 1531.5 | 1130.7 | 2662.2 | 3.5606 | 1.8718 | 5.4323 |  |
| 13 | 330.93 | 0.001567 | 0.012780 |  |  | 2476 | 1571.1 | 1066.5 | 2637.6 | 3.6232 | 1.7485 | 5.3717 |  |
| 14 | 336.75 | 0.001611 | 0.011485 | 1548.6 | 928.2 |  | 1610.5 | 1000.0 | 2810.5 | 3.6848 | 1.6249 | 5.3098 |  |
| 15 | 342.24 | 0.001658 | 0.010337 | 1585.6 |  | 7 | -1650.1 | 930.6 | 2580.6 | 3.7461 | 1.4994 | 5.2455 |  |
| 16 | 347.44 | 0.001711 | . 0093 |  |  |  | 1690.3 | 856.9 | 2547.2 | 3.8078 | 1.3698 | 5.1777 |  |
| 17 | - 352.37 | 0.001770 | 0.008364 | 1660.2 | 744.8 | 2374.3 | 17320 | 777.1 | 2509.1 | 3.8715 | .1.2329 | 5:1044 |  |
| 18 | 357.06 | 0.001840 | 0.007489 | 1698.9 | 67.4 | 2338.1 | 1776.5 | 688.0 | 2464.5 | 3.9388 | 1.0839 | 5.0228 |  |
| 19 | 361.54 | 0.001924 | 0.006657 | 1739.9 | 5075 |  | 1826.3 | 583.4 | 2409.7 | 4.0139 | 0.8130 | 4.9269 |  |
| 20 | 365.81 | 0.002036 | 0.005834 | 1785.6 | 07 | 2230.6 | 1888.4 | 446.2 | 2334.6 | 4.1075 | 0.6938 | 4.8013 |  |
| 21 | 369.89 | 0.002207 | 0.004952 | 1842.1 | 125.2 | 2087.1 | 2022.2 | 143.4 | 2165.6 | 4.3110 | 0.2216 | 4.5327 |  |
| 22 | 373.80 | 0.002742 | 0.003568 | 1020. |  | 2029.6 | 2099.3 | 0 | 2099.3 | 4.4298 | 0 | 4.4298 |  |
| 22.09 | 374.14 | 0.003155 | 0.003155 | 2029.6 | 0 |  |  |  |  |  |  |  |  |



The temperature in parontheses is the sat uration tpmperature at the specitiod pressure.
tpropertles of saturatod vapor at the speclined pressuro.
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TABLE A-G
Superheated water (Continued)


TABLEA-6


Superhented water (Continuted)

TABLE A-G

| Supierhicated water (Conclualled) |  |  |  |  |  |  |  |  |  |  |  | $\stackrel{s}{5} \mathrm{~J}(\mathrm{~kg} \cdot \mathrm{~K})$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\overline{{ }_{-C}}$ | $m^{2} / \mathrm{kg}$ | $\begin{aligned} & u \\ & \mathbf{k} J / \mathrm{kg} \end{aligned}$ | $\begin{aligned} & \mathrm{h} \\ & \mathrm{k} / \mathrm{J} / \mathrm{kg} \end{aligned}$ | $\stackrel{\mathrm{k}}{\mathrm{~kJ} / \mathrm{kg} \cdot \mathrm{Kl}}$ | ${ }^{V}{ }^{\text {m }} / \mathrm{kg}$ | kJIfkg | kJ/kg | kJ/ $/ \mathrm{kg} \cdot \mathrm{K}$ ) | $\mathrm{m}^{3} / \mathrm{kg}$ | kJ/kg |  |  |
|  | $P=15.0 \mathrm{MPa}\left(342.24^{\circ} \mathrm{C}\right]$ |  |  |  | $P=17.5 \mathrm{MPa}\left(354.75^{\circ} \mathrm{C}\right)$ |  |  |  | $P=20.0 \mathrm{MPa}\left(365.81^{\circ} \mathrm{C}\right)$ |  |  |  |
|  |  |  |  |  | 0.007920 | 2390.2 | 2528.8 | 5.1419 | 0.005834 | 2293.0 | 2409.7 | 4.9269 |
| Sat. | 0.010337 | 2455.5 | 2610.5 | 5.3098 | 0.007920 |  |  |  |  |  |  |  |
| 350 | 0.011470 | 2520.4 | 2692.4 |  | 001244 | 2685.0 | 2902.9 | 5.7213 | 0.009942 | 2619.3 | 2818.1 | 5.5540 |
| 400 | 0.015649 | 2740.7 | 2975.5 | 5.8811 | 0.012447 | 2844.2 | 3109.7 | 6.0184 | 0.012695 | 2808.2 | 3050.1 | 5.9017 |
| 450 | 0.018445 | 2879.5 | 3156.2 | 6.1404 | 0. | 2970.3 | 3274.1 | 6.2383 | 0.014768 | 2942.9 | 3238.2 | 6.1401 |
| 500 | 0.02080 | 2996.6 | 3308.6 | 6.3 |  | 3083.9 | 3421.4 | 6.4230 | 0.016555 | 3062.4 | 3393.5 | 6.3348 |
| 550 | 0.02293 | 3104.7 | 3448.6 | 6.5 | 0.01928 | 31915 | 3560.1 | 6.5866 | 0.018178 | 3174.0 | 3537.6 | 6.5048 |
| 600 | 0.02491 | 3208.6 | 35823 | 6.6776 | 0.02106 | 3296.0 | 3693.9 | 6.7357 | 0.019693 | 3281.4 | 3675.3 | 6.6582 |
| 650 | 0.02680 | 3310.3 | 3712.3 | 6.8224 | 0.02274 | 3398.7 | 3824.6 | 6.8736 : | 0.02113 | 3386.4 | 3809.0 | 6.7993 - |
| 700 | 0.02861 | 3410.9 | 3840.1 | 6.9572 | 0.02434 | 3368.8 | 4081.1 | 7.1244 | 0.02385 | 3592.7 | 4069.7 | 7.0544 |
| 800 | 0.03210 | 3610.9 | 40924 | 7.2040 | 0.02738 | 3808.7 | 4335.1 | 7.3507 | 0.02645 | 3797.5 | 4326.4 ${ }^{\text { }}$ | 7.2830 |
| 900 | 0.03546 | 3811.9 | 4343.8 | 7.4279 | 0.03031 | 4804.7 | 4589.5 | 7.5589 | 0.02897 | 4003.1 | 4582.5 | 7.4925 |
| 1000 | 0.03875 | 4015.4 | 4596.6 | 7.6348 | 0.03316 | 4016.9 | 4846.4 | 7.7531 | 0.03145 | 4211.3 | 4840.2 | 7.6874 |
| 1100 | 0.04200 | 4222.6 | 4852.6 | 7.8283 | 0.03597 | 4216.9 | 5106.6 | 7.9360 | 0.03391 | 1422.8 | 5101.0 | 7.8707 |
| 1200 | 0.04523 | 4432.8 | 5112.3 | g.010e | 0.03 L 76 | 4643.6 | 6370.5 | 8.1093 | 0.03638 | 4638.0 | 5365.1 | 8.0442 |
| 1300 | 0.04845 | 4649.1 | 5376.0 | 8.1840 | P=30.0 ${ }^{\text {a Pa }}$ |  |  |  | Pa 35.0 MPa |  |  |  |
|  | $P=25.0 \mathrm{MPP}$ |  |  |  |  | P= | , ${ }^{\text {NPa }}$ |  |  |  | 17624 | 3.8722 |
| 375 | 0.0019731 | 1788.7 | 1848.0 | 4.0320 | 0.0017892 | 1737.0 | 1791.5 | 3.8305 4.4720 | 0.0017003100 | 1914.1 | 1987.6 | 4.2126 |
| 400 | 0.006004 | 2430.1 | 2580.2 | 5.1418 | 0.002790 | 2067.4 | 2 | 5.1604 | 0.003428 | 2253.4 | 2373.4 | 4.7747 |
| 425 | 0.007881 | 2609.2 | 2806.3 | 5.4723 | 0.00530 | 2455.1 | 28 | 5.4424 | 0.004961 | 2498.7 | 2672.4 | 6.1962 |
| 450 | 0.009162 | 2720.7 | 2949.7 | 5.6744 | 0.0067 | 20 | 30 | 5.7905 | 0.006927 | 2751.9 | 2994.4 | 5.6282 |
| 500 | 0.011123 | 2884.3 | 3162.4 | 5.9592 | 0.0086 |  | 3275.4 | 6.0342 | 0.008345 | 2921.0 | 3213.0 | 5.9020 |
| 550 | 0.012724 | 3017.5 | 3335.6 | 6.1765 | 0.0101 | 5 | 3443.9 | 6.2331 | 0.009527 | 30020 | 3395.5 | 6.1179 |
| 600 | 0.014137 | 3137.9 | 3491.4 | 6.3602 | 0.0114 | 3221.0 | 3598.8 | 6.4058 | 0.010576 | 3169.8 | 3559.9 | -6.3010 |
| 650 | 0.015433 | 3251.0 | 3637.4 | 6.6229 | 0.01259 | 3735.8 | 3745.8 | 6.5606 | 0.011533 | 3309.8 | 3713.5 | 6.4631 |
| 700 | 0.016646 | 3361.3 | 3777.5 | 6.6 | 0.01366 | 3555.5 | 4024,2 | 6.8332 | 0.013278 | 3530.7 | 4001.5 | 6.7450 |
| 800 | 0.018912 | 3574.3 | 4047.1 | 6.9345 | 0.01562 | 3788.5 | 4201.9 | 7.0718 | 0.014883 | 3754,0 | 4274.8 | 6.9386 |
| 900 | 0.021045 | 3783.0 | 4309.1 | 7.1680 | 0.01744 | 3978. | 4554.7 . | 7.2867 | 0.018410 | 3966.7 | 4541.1 | 7.2004 |
| 1000 | 0.02310 | 3990.9 | 4568.5 | 7.3802 | 0:01919 | 4189.2 | 4816.9 | 7.4045 | 0.017895 | 4178.3 | 4804.6 | 7.4037. |
| 1100 | 0.02512 | 4200.2 | 4828.2 | 7.5765 | 0.0209 | 4401.3 | 5079.0 | 7:6692 | 0.018360 | . 4390.7 | 5068.3 | - 7.5910 |
| 1200 | 0.02711 | 4412.0 : | 5089.9 | 7.7 | . 2258 | 4616.0 | 6344.0 | 7.6432 | 0.020815 | 4605.1 | 6333.6 | 7.7653 |
| 1300 | 0.02910 | 4626.9 | 6354.4 | 7.934 | $P=50.0 \mathrm{MPa}$ |  |  |  | $P_{\text {mag }} 0.0 \mathrm{MPa}$ |  |  |  |
|  | $P=40.0$ RPPa |  |  |  |  | P= | , MPa |  |  |  | 1699.5 | 3.7141 |
| 375 | 0.0016407 | 1677.1 | 1742.8 | 3.8290 | 0.0015594 | 1638.6 | 1716.6 | 3.7639 4.0031 | 0.0015028 | 1745.4 | 1843.4 | 3.9318 |
| 400 | 0.0019077 | 1854.6 | 1930.9 | 4.1135 | 0.0017309 | 1788.1 | 1874.6 | 4.2734 | 0.0018165 | 1892.7 | 2001.7 | 4.1626 |
| 425 | 0.002532 | 2096.9 | 2188.1 | 4.5029 | 0.002007 | 1859.7 | 2284 | 4.5884 | 0.002085 | 2053.9 | 2179.0 | 4.4121 |
| 450 | 0.003693 | 2365.1 | 25120 | 4.9459 | 0.002486 | 2159.6 |  | 5.1726 | 0.002956 | 2390.6 | 2567.9 | 4.9321 |
| 600 | 0.005622 | 2678.4 | 2903.3 | 5.4700 | 0.003892 | 5. | 3019.6 | 5.5465 | 0.003958 | 2658.8 | 2896.2 | 5.9441 |
| 550 | 0.006984 | 2869.7 | 3149.1 | 6.7785 | 0.005118 | 2763.6 | 3247.6 | 6.8178 | 0.004934 | 2861.1 | 31512 | 5.6452 |
| 600 | 0.008094 | 3022.6 | 3346.4 | 6.0144 | 0.006112 | 29433.5 | 3441.8 | 6.0342 | 0.005595 | 3028.8 | 3364.5 | 5.8829 |
| 650 | 0.009063 | 3158.0 | 3520.6 | 6.2054 | 0.00696 | 3230.5 | 3816.8 | 0.2189 | 0.006272 | 3171.2 | '3553. 5 | 0.0824 |
| 700 | 0.009941 | 3283.6 | 3681.2 | 6.3750 | 0.00772 | 3479.8 | 3933.8 | 6.6290 | 0.007459 | 3441.5 | 3869.1 | 6.4109 |
| 800 | 0.011523 | 3517.8 | 3978.7 | 0.6682 | 0.00907 | 3710.3 | 4224.4 | 0.7882 | 0.008508 | 3681.0 | 4191.5 | 6.6805 |
| 900 | 0.012962 | 3739.4 | 4257.9 | 6.9150 | 0.01028 | 3930.5 | 4501.1 | 7.0146 | 0.009480 | 3900.4 | 4475.2 | 6.9127 |
| 1000 | 0.014324 | 3954.6 | 4527.6 | 7.1356 | 0.011411 | 4145.7 | 4770.5 | 7,2184 | 0.010409 | 4124.1 | 4746.6 | 7.1195 |
| 100 | 0.015642 | 4167.4 | 4793.1 | 7.3364 | 0.012436 | 4185.7 | 60372 | 7.4058 | 0.011317 | 4388.2 | 5017.2 | 7.3093 |
| 1200 | 0.016940 | 4380.1 | 5057.7 | 7.5224 | 0.013561 |  | 5303.6 | 7.5808 | 0.012215 | 4551.4 | 5284.3 | 7.4837 |
| 1300 | 0.018229 | 4594.3 | 5323.5 | 7.6969 | 0.014616 | 4572 |  |  |  |  |  |  |

TABLE A-T.
Compiressed liquid water


TABLEA-11

| $\begin{aligned} & \text { Tomp., } \\ & T^{*} \mathrm{C} \end{aligned}$ | Press., $P_{s a l}$ MPa | Specific volume, $\mathrm{m}^{3} / \mathrm{kg}$ |  | $\begin{gathered} \text { Internal } \\ \text { energy, } \mathrm{kJ} / \mathrm{kg} \end{gathered}$ |  | $\begin{aligned} & \text { Enthalpy } \\ & \mathrm{kJ} / \mathrm{kg} \end{aligned}$ |  |  | $\begin{aligned} & \text { Entrop } y_{\mathrm{s}} \\ & \mathrm{KJ} /(\mathrm{kg} \cdot \mathrm{~K}) \\ & \hline \end{aligned}$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | Sat. IIquid, v, | Sat. vapor, $v_{0}$. | Sat. <br> liquid, $u_{f}$ | Sat. vapor, $u_{g}$ | Sat. liquid, $h$ | Evap., $h_{\text {lg }}$ | Sat. vapor, $b_{g}$ | Sat. <br> liquid $S_{1}$ | Sat. vapor, $s_{p}$ |
|  |  |  |  |  |  | 0.00 | 222.88 | 222.88 | 0.0000 | 0.9560 |
| -40 | 0.05164 | 0.0007055 | 0.3569 | -0.04 | 204.45 | 4.73 | 220.67 | 225.40 | 0.0201 | 0.9506 |
| -36 | 0.06332 | 0.0007113 | 0.2947 | 4.68 | 209.01 | 9.52 | 218.37 | 227.90 | 0.0401 | 0.9456 |
| -32 | 0.07704 | 0.0007172 | 0.2451 | 9.47 | 211.29 | 14.37 | 216.01 | 230.38 | 0.0600 | 0.9411 |
| -28 | 0.09305 | 0.0007233 | 0.2052 | 14.31 | 211.29 212.43 | 16.82 | 214.80 | 231.62 | 0.0699 | 0.9390 |
| -26 | 0.10199 | 0.0007265 | 0.1882 | 16.75 |  |  | 213.57 | 232.85 | 0.0798 | 0.9370 |
| -24 | 0.11160 | 0.0007296 | 0.1728 | 19.21 |  | 19.29 21.77 | 212.32 | 234.08 | 0.0897 | 0.9351 |
| -22 | 0.12192 | 0.0007328 | 0.1590 | 21.68 | 215.84 | 24.26 | 211.05 | 235.31 | 0.0996 | 0.9332 |
| -20 | 0.13299 | 0.0007361 | 0.1464 | 24.17 | 216.97 | 26.77 | 209.76 | 236.53 | 0.1094 | 0.9315 |
| -18 | 0.14483 | 0.0007395 | 0.1350 | 26.67 | 216.97 218.10 | 29.30 | 208.45 | 237.74 | 0.1192 | 0.9298 |
| -16 | 0.15748 | 0.0007428 | 0.1247 | 29.18 |  |  | 205.77 | 240.15 | 0.1388 | 0.9267 |
| -12 | 0.18540 | 0.0007498 | 0.1068 | 34.25 | 22 | 34.54 | 203.00 | 242.54 | 0.1583 | 0.9239 |
| -8 | 0.21704 | 0.0007569 | 0.0919 | 39.38 | 222.60 | 44.75 | 200.15 | 244.90 | 0.1777 | 0.9213 |
| -4 | 0.25274 | 0.0007644 | 0.0794 | 44.56 | 224.84 227.06 | 50.02 | 197.21 | 247.23 | 0.1970 | 0.9190 |
| 0 | 0.29282 | 0.0007721 | 0.0689 | 49.79 | 227.06 229.27 | 55.35 | 194.19 | 249.53 | 0.2162 | 0.9169 |
| 4 | 0.33765 | 0.0007801 | 0.0600 | 55.08 | 229. | 60.73 | 191.07 | 251.80 | 0.2354 | 0.9150 |
| 8. | 0.38756 | 0.0007884 | 0.0525 | 60.43 |  | $\begin{aligned} & 60.13 \\ & 66.18 \end{aligned}$ | 187.85 = | 254.03 | 0.2545 | 0.9132 |
| 12 | 0.44294 | 0.0007971 | 0.0460 | 65.83 | 235.78 | 71.69 | 184.52 | 256.22 | 0.2735 | 0.9116 |
| 16 | 0.50416 | 0.0008062. | 0.0405 | 71.29 | 235.781 | 77.26 | 181.09 | 258.35 | 0.2924 | 0.9102 |
| 20 | 0.57160 | $0.0008157{ }^{\circ}$ | 0.0358 | 8237 | 240.01 | 77.2 | 177.55 | 260.45 | 0.3113 | 0.9088 |
| 24 | 0.64566 | 0.0008257 | 0.0317 | 82.37 | 240.01 |  |  | 261.48 | 0.3208 | 0.9082 |
| 26 | 0.68530 | 0:0008309 | 0.0298 | 85.18 | 241.05 | 88:61 | $173.89$ | 262.50 | 0.3302 | 0.9076 |
| 28 | 0.72675 | 0.0008362 | 0.0281 | 88.00 | 242.08 | 81.49 | 172.00 | 263.50 | 0.3396 | 0.9070 |
| 30 | 0.77006 | 0.0008417 | 0.0265 | 84 | 243.10 | 94.39 . | 170.09 | 264.48 | 0.3490 | 0.9064 |
| 32 | 0.81528 | 0.0008473 | 0.0250 | 93.70 | 244.12 | 97.31 | 168.14 | 265.45 | 0.3584 | 0.9058 |
| 34 | 0.86247 | 0.0008530 | 0.0236 | 96.58 |  |  |  |  | 0.3678 | 0,9053 |
| 36 | 0.91168 | . 0.0008590 | 0.0223 | 99.47 | 246.11 | $103.21$ | 164.12 | 267.33 | 0.3772 | 0.9047 |
| 38 | 0.96298 | 0.0008651 | 0.0210 | 102.38 |  | 106.19 | 162.05 | 268.24 | 0.3886 | 0.9041 |
| 40 | 1.0164 | 0.0008714 | 0.0199 | 105.30 | 249.02 | 109.19 | 159.94 | 269.14 | 0.3960 | 0.9035 |
| 42 | 1.0720 | 0.0008780 | 0.0188 | 108 | 24 | 112.22 | 157.79 | 270.01 | 0.4054 | 0.9030 |
| 44 | 1.1299 | 0.0008847 | 0.0177 | 111.22 |  |  |  | 88 | 0.4243 | 0.9017 |
| 48 | 1.2526 | 0.0008989 | 0.0159 | 117.22 | 251.79 |  | 148.66 | 273.24 | 0.4432 | 0.9004 |
| 52 | 1.3851 | 0.0009142 | 0.0142 | 23 |  | $\cdot 13$ | 143.75 | 274.68 | 0.4622 | 0.8990 |
| 56 | 1.5278 | 0.0009308 | 0.0127 | 129.51 | 255.23 | 137.42 | 138.57 | 275.99 | 0.4814 | 0.8973 |
| 60 | 1.6813 | 0.0009488 | 0.0114 | 135:82 |  |  |  | 43 | 0.5302 | 0.8918 |
| 70 | 21162 | 0.0010027 | 0.0086 | 152.22 | 26 | $154 .$ | 106.41 | 279.12 | 0.5814 | 0.8827 |
| 80 | 2.6324 | 0.0010766 | 0.0064 | 169.88 | 26.14 | 193.69 | 82.63 | 276.32 | 0.6380 | 0.8655 |
| 90 | 3.2435 | 0.0011949 | 0.0046, | 189.8 | 261.34 | 153.69 | 34.40 | 259.13 | 0.7196 | 0.8117 |
| 100 | 3.9742 | 0.0015443 | 0.0027 | 21 | 248.4 |  |  |  |  |  |

. Source for Tables A-8 through A-10: M. J. Moran and H. N. Shapiro, FU irom D. P. Wilson and R. S. Basu, "Thiermödynamle Properities ol a John Willey \& Sons, 1992), pp, 710-15. Orighany basodi Now Stratospherlcally Sale Wöking Fluld- Relfigerant-134a," ASHRA 916

| Salurated refrigerant-134a_Pressure table Spocifle volume, $\mathrm{m}^{3} / \mathrm{kg}$ |  |  |  | $\begin{aligned} & \text { Internal } \\ & \text { energy, } \mathrm{k} / \mathrm{kg} \end{aligned}$ |  | Enthalpy: $\mathrm{kJ} / \mathrm{kg}$ |  |  | $\begin{aligned} & \text { Entropy, } \\ & \mathrm{KJ}(\mathrm{~kg} \cdot \mathrm{~K}) \end{aligned}$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  |  |  |  | Sat. | Sat. |  |
|  | Temp., | Sat. <br> Ilquid, | Sat. vapor, |  |  | Sat. <br> liquid, | vapor, | liquid, $h_{1}$ | Evap., $h_{\text {f }}$ | vapor, <br> $h_{0}$ | $\begin{aligned} & \text { liquid } \\ & s_{f} \end{aligned}$ | $\begin{aligned} & \text { vapor } \\ & s_{0} \\ & \hline \end{aligned}$ |
| Press.g <br> PMPa | $T_{\text {cat }}{ }^{\circ} \mathrm{C}$ | $v_{f}$ | $v_{0}$ | $u_{1}$ |  | $h_{\text {f }} 3.46$ | 221.27 | 224.72 | 0.0147 | 0.9520 |
| 0.06 | -37.07 | . 0.0007097 | 0.3100 | 3.41 | 206.12 | 10.47 | 217.92 | 228.39 | 0.0440 | 0.9447 |
| 0.08 | -31.21 | 0.0007184 | 0.2366 | 10.41 | 212.18 | 16.29 | 215.06 | 231.35 | 0.0678 | 0.9395 |
| 0.10 | -26.43 | 0.0007258 | 0.1917 | 16.22 | - | 21.32 | 212.54 | 233.86 | 0.0879 | 5 |
| 0.12 | -22.36 | - 0.0007323 | 0.1614 | 21.23 | 216.52 | 25.71 | 210.27 | $236.04{ }^{\prime}$ | 0.1055 | 0.9322 |
| 0.14 | -18.80 | 0.0007381 | 0.1395 | 25.66 |  | 29.78 | 208.18 | 237.97 | 0.1211 | 0,9295 |
| 0.16 | -15.62 | 0.0007435 | 0.1223 | 29.66 | 21 | 33.45 | 206.26 | 239.71 | 0.1352 | 0.9273 |
| 0.18 | -12.73 | 0.0007485 | 0.1098 | 33.31 | 21.94 | 36.84 | 204.46 | 241.30 | 0.1481 | 0.9253 |
| 0.20 | -10.09 | 0.0007532 | 0.0993 | 36.69 | 224.07 | 42.95 | 201.14 | 244.09 | 0.1710 | 0.9222 |
| 0.24 | -5.37 | 0.0007618 | . 083 | 2.77 | 226.38 | 48.39 | 198.13 | 246.52 | 0.1911 | 0.9197 |
| 0.28 | -1.23 | 0.0007697 | 0.0719 | 48.18 | 226.38 | 53.31 | 195.35 | 248.66 | 0.2089 | 0.9177 |
| 0.32 | 2.48 | 0.0007770 | 0.0632 | 53 |  | 57.82 | 192.76 | 250.58 | 0.2251 | 0.9160 |
| 0.36 | 5.84 | 0.0007839 | 0.0564 | 57.54 | 231.97 | 62.00 | 190.32 | 252.32 | 0.2399 | 0.9145 |
| 0.4 | 8.93 | 0.0007904 | 0.0509 | 61.69 | 235.64 | 71.33 | 184.74 | 256.07 | 0.2723 | 0.9117 |
| 0.5 | 15.74 | 0.0008056 | 0.0409 | 70.93 | 238.74 | 79.48 | 179.71 | 259.19 | 0.2999 | 0.9097 |
| 0.6 | 21.58 | 0.0008196 | 0.0341 | 78.99 |  | 86.78 | 175.07 | 261.85 | 0.3242 | 0.9080 |
| 0.7 | 26.72 | 0.0008328 | 0.0292 | 86.19 | 243.78 | 93.42 | 170.73 | 264.15 | 0.3459 | 0.9066 |
| 0.8 | $31.33{ }^{\circ}$ | 0.0008454 | 0.0255 | 9 | 245.88 | 99.56 | 168.62 | 266.18 | 0.3656 | 0.9054 |
| 0.9 | 35.53 | 0.0008576 | 0.0226 | 98.79 | 247.77 | 105.29 | 162.68 | 267.97 | 0.3838 | 0.9043 |
| 1.0 | 39.39 | 0.0008695 | 0.0202 | 104.42 | 251.03 | 115.76 | 155.23 | 270.99 | 0.4164 | 0.9023 |
| 1.2 | 46.32 | 0.0008928 | 0.0 |  |  | 125.26 | 148.14 | 273.40 | 0.4453 | 0.9003 |
| 1.4 | 52.43 | 0.0009159 | 0.0140 | 123.98 |  | 134.02 | 141.31 | 275.33 | 0.4714 | 0.8982 |
| 1.6 | 57.92 | 0.0009392 | 0.0121 | 132.5 | $257.88^{\circ}$ | 142.22 | 134.60 | 276.83 | 0.4954 | 0.8959 |
| 1.8 | 62.91 | 0.0009631 | 0.0105 | 140.49 | 259.41 | 149.99 | 127.95 | 277.94 | 0.5178 | 0.8934 |
| 2.0 | 67.49 | 0.0009878 | 0.0093 | 148.02 | 261.84 | 168.12 | 111.06 | 279.17 | 0.5687 | 0.8854 |
| 2.5 | . 77.59 | 0.0010562 | 0.0069 | 165.48 | 262.16 | 185.30 | 92.71 | 278.01 | 0.6156 | 0.8735 |
| 3.0 | 86.22 | 0.0011416 | 0.0053 | 181.08 |  |  |  |  |  |  |

TABLEA-13


TABLEA-13



Source: Adapled from K. Wark. Thernadÿnamics. 4ih ed., McGraw.Hill, New York.t1983, as bascd on "Tables of Thermal Properiles of Gascs," NBS Circular 564, 1955.
table A-17 Ideal Gas Propertics of Nilrogen, $\mathrm{N}_{2}$
$T(\mathrm{~K}), \bar{h}$ and $\bar{\pi}(\mathrm{kJ} / \mathrm{kmol}), \bar{s}^{\circ}(\mathrm{kJ} / \mathrm{kmol} \cdot \mathrm{K})$
$\left[\bar{h}_{f}^{0}=0 \mathrm{~kJ} / \mathrm{kmol}\right]$

| $T$ | $\bar{h}$ | $\bar{u}$ | ${ }^{\circ}$ |
| :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 0 |
| 220 | 6,391 | 4.562 | 182.639 |
| 230 | 6,683 | 4,770 | 181.938 |
| 240 | 6.975 | 4,979 | 185.180 |
| 250 | 7.266 | 5,188 | 186.370 |
| 260 | 7,558 | 5,396 | 187.514 |
| 270 | 7,849 | 5,604 | 188.614 |
| 280 | 8,141 | 5,813 | 189.673 |
| 290 | 8,432 | 6.021 | 190.695 |
| 298 | 8,669 | 6,190 | 191.502 |
| 300 | 8,723 | 6.229 | 191.682 |
| 310 | 9;014 | 6,437 | 192.638 |
| 320 | 9.306 | 6,645 | 193.562 |
| 330 | 9,597 | 6,853 | 194.459 |
| 340 | 9,888 | 7,061 | 195.328 |
| 350 | 10,180 | 7,270 | 196.173 |
| 360 | 10.471 | 7.478 | 196.995 |
| 370 | 10,763 | 7,687 | 197.794 |
| 380 | 11,055 | 7,895 | 198.572 |
| 390 | 11,347 | 8,104 | 199.331 |
| 400 | 11,640 | 8,314 | 200.071 |
| 410 | 11,932 | 8,523 | 200.794 |
| 420 | 12,225 | 8,733 | 20.489 |
| 430 | 12,518 | 8.943 | 202.189 |
| 440 | 12.811 | 9,153 | 202.863 |
| 450 | 13,105 | 9,363 | 203.523 |
| 460 | 13,399 | 9.574 | 204.170 |
| 470 | 13,69] | 9.786 | 204.801 |
| 480 | 13,988 | 9,997 10,210 | 205.424 206.033 |
| 490 | 14.285 | 10,210 | 206.033 |
| 501 | 14,581 | 10,423 | 206.630 |
| 510 | 14,876 | 10,635 | 207.21 |
| 520 | 15,172 | 10,848 | 207.792 |
| 530 | 15,469 | 11,062 | 208.358 |
| 540 | 15,766 | 11,277 | 208.91 |
| 550 | 16,064 | 11,492 | 209.46 |
| S60 | 16,363 | 11,707 | 209.95 |
| 570 | 16,662 | 11.923 | 210.52 |
| 580 | 16,462 | 12,139 | 211.04 |
| 580 | 17,262 | 12.356 | 211.56 |


| $T$ | $\bar{h}$ | \# | $5^{\circ}$ |
| :---: | :---: | :---: | :---: |
| 600 | 17,563 | 12.574 | 212.066 |
| 610 | 17,864 | 12,792 | 212.564 |
| 620 | 18,166 | 13.011 | 213.055 |
| 630 | 18,468 | 13,230 | 213.541 |
| 640 | 18,772 | 13.450 | 214.018 |
| 650 | 19,075 | 13,671 | 214.489 |
| 660 | 19,380 | 13.892 | 214.954 |
| 670 | 19,685 | 14,114 | 215.413 |
| 680 | 19,991 | 14,337 | 5.866 |
| 690 | 20,297 | 14,560 | 216.314 |
| 700 | 20,604 | 14,784 | 216.756 |
| 710 | 20,912 | 15,008 | 7.192 |
| 720 | 21,220 | 15,234 | 217.624 |
| 710 | 21,529 | 15.460 | 218.059 |
| 740 | 21,839 | 15.686 | 218.472 |
| 750 | 22,149 | 15,913 | 218.889 |
| 760 | 22,460 | 16,141 | 219.301 |
| 770 | 22,712 | 16,370 | 219.709 |
| 780 | 23,085 | 16,599 | 220.113 |
| 790 | 23,398 | .16.830 | 220.512 |
| 800 | 23,714 | 17.061 | 220.907 |
| 810 | 24,027 | 17,292 | 221.298 |
| 820 | 24,342 | 17,524 | 221.684 |
| 830 | 24,658 | 17.757 | 222.067 |
| 840 | 24,974 | 17.990 | 222.447 |
| 850 | 25,292 | 18,224. | 222.822 |
| 860 | 25,610 | 18,459 | 223.194 |
| 870 | 25,928 | 18,695 | 223.562 |
| 880 | 26,248 | 18.931 | 223.927 |
| 890 | 26,568 | 18,168 | 224.288 |
| 900 | 26,890 | 19.407 | 224.647 |
| 910 | 27,210 | 19,644 | 225.002 |
| 920 | 27,532 | 19,883 | 225.351 |
| 930 | 27,854 | 20,122 | 225.701 |
| 940 | 28,178 | 20,362 | 226.047 |
| 950 | 28,501 | 20,603 | 226.389 |
| 960 | 28,826 | 20,844 | 226.728 |
| 970 | 29.151 | 21,086 | 227.064 |
| 980 | 29.476 | 21,328 | 227 |
| 990 | 29.803 | 21.571 | 227.7 |

$z$

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Table A-18 Ideal Gas Properies of Oxygen, $\mathrm{O}_{2}$
$T(\mathrm{~K}), \bar{h}$ and $\tilde{u}(\mathrm{~kJ} / \mathrm{kmol}), \mathcal{J}^{\circ}(\mathrm{kJ} / \mathrm{kmol} \cdot \mathrm{K})$

$$
\left[\bar{h}_{j}^{0}=0 \mathrm{~kJ} / \mathrm{kmol}\right]
$$

| $T$ | $\bar{h}$ | $\overline{4}$ | $5^{\circ}$ |
| :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | $\bigcirc$ |
| 220 | 6,404 | 4.575 | 196.171 |
| 230 | 6,694 | 4.782 | 197.461 |
| 240 | 6.984 | 4,989. | 198.696 |
| 250 | 7.275 | 5.197 | 199.885 |
| 260 | 7,566 | 5,405 | 201.027 |
| 270 | 7.858 | 5,613 | 202.128 |
| 280 | 8,150 | 5.822 | 203.191 |
| 290 | 8,443 | 6,032 | 204.218 |
| 296 | 8.682 | 6.203 | 205.033 |
| 100 | 8,736 | 6.242 | 205.213 |
| 310 | 9,010 | 6,453 | 206. 177 |
| 330 | 9.325 | 6.664 | 207.112 |
| 330 | 9.620 | 6.877 | 208.020 |
| 340 | 9.916 | 7,090 | 208.904 |
| 350 | 10,2!3 | 7,303 | 209.765 |
| 360 | 10,511 | 7.518 | 210.604 |
| 370 | 10.809 | 7,733 | 211.423 |
| 380 | 11,109 | 7.949 | 212.222 |
| 390 | 11,409 | 8,166 | 213.002 |
| 400 | 11.751 | 8,384 | 213.765 |
| 410 | 12,012 | 8.603 | 214.510 |
| 420 | 12.314 | 8,822 | 215.241 215.955 |
| 430 | 12,618 | 9,043 9.264 | 215.955 216.656 |
| 440 | 12,923 | 9.264 | 216.656 |
| 450 | 13,228 | 9.487 | 217.342 |
| 460 | 13.535 | 9.710 | 218.016 |
| 470 | 13,842 | 9.935 | 218.676 |
| 480 | 14,151 | 10,160 | 219.326 |
| 490 | 14,460 | 10,386 | 219.963 |
| 500 | 14.770 | 10,614 | 220.589 |
| 510 | 15,082 | 10,842 | 221.206 |
| 520 | 15,395 | 11,071 | 221.812 |
| 5311 | 15,708 | 11,301 | 222.409 |
| 540 | 16,022 | 11,5, 3 | 222.997 |
| 550 | 16,338 | 11.765 | 223.576 |
| 5510 | 16,654 | 11,998 | 124.146 |
| 570 | 16.971 | 12,232 | 224.708 |
| 580 | 17,290 | 12,467 | 225.262 |
| 590 | 17.609 | 12,703 | 225.808 |


| $T$ | $\bar{h}$ | u | $5^{\circ}$ |
| :---: | :---: | :---: | :---: |
| 600 | 17,929 | 12.940 | 226.346 |
| 610 | 18,250 | 13.178 | 226.877 |
| 620 | 18,572 | 13.417 | 227.400 |
| 630 | 18,895 | 13,657 | 227.918 |
| 640 | 19,219 | 13,898 | 228.429 |
| 650 | 19,544 | 14,140 | 228.032 |
| 660 | 19,870 | 14,383 | 229.430 |
| 670 | 20,197 | 14,626 | 229.920 |
| 680 | 20,524 | 14,871 | 230.405 |
| 690 | 20,854 | 15,116 | 230.885 |
| 700 | 21,184 | 15,364 | 231.358 |
| 710 | 21,514 | 15,611 | 231.827 |
| 720 | 21,845 | 15,859 | 232.291 |
| 730 | 22,177 | 16.107 | 232.748 |
| 740 | 22,510 | 16,357 | 231.201 |
| 750 | 22,844 | 16,607 | 233.649 |
| 760 | 23,178 | 16,859 | 234.091 |
| 770 | 23,513, | 17,111 | 234.528 |
| 780 | 23,850 | 17,364 | 234.960 |
| 790 | 24,186. | 17,618 | 235.387 |
| 800 | 24,523 | 17,872 | 235.810 |
| 810 | 24,861 | 18,126 | 236.230 |
| 820 | 25, 199 | 18,382 | 236.644 |
| 830 | 25,537 | 18,637 | 237.055 |
| 840 | 25.877 | 18,893 | 237.462 |
| 850 | 26,218 | 19,150 | 237.864 |
| 860 | 26,559 | 19,408 | 238.264 |
| 870 | 26,899 | 19,666 | 238.660 |
| 880 | 27,242 | 19,925 | 239.051 |
| 890 | 27,584 | 20,185 | 239.439 |
| 900 | 27,928 | 20,445 | 239.821 |
| 910 | 28,272 | 20,706 | 240.201 |
| 920 | 28,616 | 20,967 | 240.580 |
| 930. | 28,960 | 21.228 | 240.953 |
| 940 | 29,306 | 21,491 | 241.323 |
| 950 | 29,652 | 21,754 | 241.689 |
| 960 | 29,999 | 22,017 | 242052 |
| 970 | 30,345 | 22,280 | 242411 |
| 980 | 30,692 | 22,544 | 242.768 |
| 990 | 31,041 | 22.809 | 243.120 |

TAbLE A- 19 Idcal Gas Properties of Walcr Vapor, $\mathrm{H}_{2} \mathrm{O}$
$T(\mathrm{~K}), \overline{\mathrm{h}}$ and $\widetilde{u}(\mathrm{~kJ} / \mathrm{kmol}) \dot{\bar{s}}^{\mathrm{s}}(\mathrm{kJ} / \mathrm{kmol} \cdot \mathrm{K})$
$\left[\vec{h}_{\rho}^{0}=-241,820 \mathrm{~kJ} / \mathrm{kmol}\right]$

TABLE A-22 Ideal Gas Properties of Air

| $T(\mathrm{~K}), h$ and $u(\mathrm{~kJ} / \mathrm{kg}), s^{\circ}(\mathrm{kJ} / \mathrm{kg} \cdot \mathrm{K})$ |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $T$ | $h$ | P, | 4 | $0^{\prime}$ | 5 | T | h | p. | $u$ | Dr | ת |
| 200 | 199.97 | 0.3363 | 142.56 | 1707. | 1.29559 | 450 | 451.80 | 5.775 | 322.62 | 223.6 | 2.11161 |
| 210 | 209.97 | 0.3987 | 149.69 | 1512. | 1.34444 | 460 | 462.02 | 6.245 | 329.97 | 211.4 | 2.13407 |
| 220 | 219.97 | 0.4690 | 156.82 | 1346. | 1.39105 | 470 | 472.24 | 6.742 | 337.32 | 200.1 | 2.15604 |
| 230 | 230.02 | 0.5477 | 164.00 | 1205. | 1.43557 | 480 | 482.49 | 7.268 | 344.70 | 189.5 | 2.17760 |
| 240 | 240.02 | 0.6355 | 171.13 | 1084. | 1.47824 | 490 | 492.74 | 7.824 | 352.08 | 179.7 | 2.19876 |
| 250 | 250.05 | 0.7329 | 178.28 | 979. | 1.51917 | 500 | 503.02 | 8.411 | 359.49 | 170.6 | 2.21952 |
| 260 | 260.09 | 0.8405 | 185.45 | 887.8 | 1.55848 | 510 | 513.32 | 9.031 | 366.92 | 162.1 | 2.23993 |
| 270 | 270.11 | 0.9590 | 192.60 | 808.0 | 1.59634 | 520 | 523.63 | 9.684 | 374.36 | 154.1 | 2.25997 |
| 280 | 280.13 | 1.0889 | 199.75 | 738.0 | 1.63279 | 530 | 533.98 | 10.37 | 381.84 | 146.7 | 2.27967 |
| 285 | 285.14 | 1.1584 | 203.33 | 706.1 | 1.65055 | 540 | 544.35 | 11.10 | 389.34 | 139.7 | 2.29906 |
| 290 | 290.16 | 1.2311 | 206.91 | 676.1 | 1.66802 | 550 | 554.74 | 11.86 | 396.86 | 133.1 | 2.31809 |
| 295 | 295.17 | 1.3068 | 210.49 | 647.9 | 1.68515 | 560 | 565.17 | 12.66 | 404.42 | 127.0 | 2.33685 |
| 300 | 300.19 | 1.3860 | 214.07 | 621.2 | 1.70203 | 570 | 575.59 | 13.50 | 411.97 | 121.2 | 2.35531 |
| 305 | 305.22 | 1.4686 | 217.67 | 596.0 | 1.71865 | 580 | 586.04 | 14.38 | 419.55 | 115.7 | 2.37348 |
| 310 | 310.24 | 1.5546 | 221.25 | 572.3 | 1.73498 | 590 | 596.52 | 15.31 | 427.15 | 110.6 | 2.39140 |
| 315 | 315.27 | 1.6442 | 224.85 | 549.8 | 1.75106 | 600 | 607.02 | 16.28 | 434.78 | 105.8 | 2.40902 |
| 320 | 320.29 | 1.7375 | 228.42 | 528.6 | 1.76690 | 610 | 617.53 | 17.30 | 442.42 | 101.2 | 2.42644 |
| 325 | 325.31 | 1.8345 | 232.02 | 508.4 | 1.78249 | 620 | 628.07 | 18.36 | 450.09 | 96.92 | 2.44356 |
| 330 | 330.34 | 1.9352 | 235.61 | 489.4 | 1.79783 | 630 | 638.63 | 19.84 | 457.78 | 92.84 | 2.46048 |
| 340 | 340.42 | 2.149 | 242.82 | 454.1 | 1.82790 | 640 | 649.22 | 20.64 | 465.50 | 88.99 | 2.47716 |
| 350 | 350.49 | 2.379 | 250.02 | 422.2 | 1.85708 | 650 | 659.84 | 21.86 | 473.25 | 85.34 | 2.49364 |
| 360 | 360.58 | 2.626 | 257.24 | 393.4 | 1.88543 | 660 | 670.47 | 23.13 | 481.01 | 81.89 | 2.50985 |
| 370 | 370.67 | 2.892 | 264.46 | 367.2 | 1.91.313 | 670 | 681.14 | 24.46 | 488.81 | 78.61 | 2.52589 |
| 380 | 380.77 | 3.176 | 271.69 | 343.4 | 1.94001 | 680 | 691.82 | 25.85 | 496.62 | 75.50 | 2.54175 |
| 390 | 390.88 | 3.481 | 278.93 | 321.5 | 1.96633 | 690 | 702.52 | 27.29 | 504.45 | 72.56 | 2.55731 |
| 400 | 400.98 | 3.806 | 286.16 | 301.6 | 1.99194 | 700 | 713.27 | 28.80 | 512.33 | 69.76 | 2.57277 |
| 410 | 411.12 | 4.153 | 293.43 | 283.3 | 2.01699 | 710 | 724.04 | 30.38 | 520.23 | 67.07 | 2.58810 |
| 420 | 421.26 | 4.522 | 300.69 | 266.6 | 2.04142 | 720 | 734.82 | 32.02 | 528.14 | 64.53 | 2.60319 |
| 430 | 431.43 | 4.915 | 307.99 | 251.1 | 2.06533 | 730 | 745.62 | 33.72 | 536.07 | 62.13 | 2.61803 |
| 440 | 441.61 | 5.332 | 315.30 | 236.8 | 2.08870 | 740 | 756.44 | 35.50 | 544.02 | 59.82 | 2.63280 |


TABLE A-22 (Continued)

| $T(\mathrm{~K}), h$ and $\mu(\mathrm{kJ} / \mathrm{kg}), s^{\bullet}(\mathrm{kJ} / \mathrm{kg} \cdot \mathrm{K})$ |  |  |  | $v_{1}$ | 5 | $T$ | $h$ | $p$, | 4 | $u$. |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $T$ | $h$ | Pr | $\boldsymbol{4}$ |  |  |  |  |  |  |  | $5{ }^{\circ}$ |
| 750 | 767.29 | 37.35 | 551.99 | 57.63 | 2.64737 |  |  |  |  |  |  |
| 760 | 778.18 | 39.27 | 560.01 | 55.54 | 2.66176 | 1300 | 1395.97 1419.76 | 330.9 352.5 | 1022.82 | 11.275 | 3.27345 |
| 770 | 789.11 | 41.31 | 568.07 | 53.39 | 2.67595 | 1340 | 1419.76 1443.60 | 352.5 375.3 | 1040.88 1058.94 | 10.747 10.247 | 3.29160 3.30959 |
| 780 | 800.03 | 43.35 | 576.12 | 51.64 | 2.69013 | 1360 | 1467.49 | 399.1 | 1077.10 | 10.247 9.780 | 3.30959 3.32724 |
| 790 | 810.99 | 45.55 | 584.21 | 49.86 | 2.70400 | 1380 | 1491.44 | 424.2 | 1095.26 | 9.337 | 3.34474 |
| 800 | 821.95 | 47.75 | 592.30 | 48.08 | 2.71787 | 1400 | 1515.42 | 450.5 |  |  |  |
| 820 | 843.98 | 52.59 | 608.59 | 44.84 | 2.74504 | 1420 | . 1539.44 | 478.0 | 1113.52 1131.77 | 8.919 8.526 | 3.36200 . |
| 840 | 866.08 | 57.60 | 624.95 | 41.85 | 2.77170 | 1440 | 1563.51 | 506.9 | 1150.13 | 8.526 8.153 | 3.39586 |
| 860 | 888.27 | 63.09 | 641.40 | 39.12 | 2.79783 | 1460 | 1587.63 | 537.1 | 1168.49 | 7.801 | 3.41247 |
| 880 | 910.56 | 68.98 | 657.95 | 36.61 | 2.82344 | 1480 | 1611.79 | 568.8 | 1186.95 | 7.468 | 3.42892 |
| 900 | 932.93 | 75.29 | 674.58 | 34.31 | 2.84856 | 1500 | 1635.97 | 601.9 | 1205.41 | 7.152 | 3.44516 |
| 920 | 955.38 | 82.05 | 691.28 | 32.18 | 2.87324 | 1520 | 1660.23 | 636.5 | 1223.87 | 6.854 | 3.46120 |
| 940 | 977.92 | 89.28 | 708.08 | 30.22 | 2.89748 | 1540 | 1684.51 | 672.8 | 1242.43 | 6.569 | 3.47712 |
| 960 | 1000.55 | 97.00 | 725.02 | 28.40 | 2.92128 | 1560 | 1708.82 | 710.5 | 1260.99 | 6.301 | 3.49276 |
| 980 | 1023.25 | 105.2 | 741.98 | 26.73 | 2.94468 | 1580 | 1733.17 | 750.0 | 1279.65 | 6.046 | 3.50829 |
| 1000 | 1046.04 | 114.0 | 758.94 | 25.17 | 2.96770 | 1600 | 1757.57 | 791.2 | 1298.30 | 5.804 | 3.52364 |
| 1020 | 1068.89 | 123.4 | 776.10 | 23.72 | 2.99034 | 1620 | 1782.00 | 834.1 | 1316.96 | 5.574 | 3.53879 |
| 1040 | 1091.85 | 133.3 | 793.36 | 22.39 | 3.01260 | 1640 | 1806.46 | 878.9 | 1335.72 | 5.355 | 3.55381 |
| 1060 | 1114.86 | 143.9 | 810.62 | 21.14 | 3.03449 | 1660 | 1830.96 | 925.6 | 1354.48 | 5.147 | 3.56867 |
| 1080 | 1137.89 | 155.2 | 827.88 | 19.98 | 3.05608 | 1680 | 1855.50 | 974.2 | 1373.24 | 4.949 | 3.58335 |
| 1100 | 1161.07 | 167.1 | 845.33 | 18.896 | 3.07732 | 1700 | 1880.1 | 1025 | 1392.7 | 4.761 | 3.5979 |
| 1120 | 1184.28 | 179.7 | 862.79 | 17.886 | 3.09825 | 1750 | 1941.6 | 1161 | 1439.8 | 4.328 | 3.6336 |
| 1140 | 1207.57 | 193.1 | 880.35 | 16.946 | 3.11883 | 1800 | 2003.3 | 1310 | 1487.2 | 3.944 | 3.63884 |
| 1160 | 1230.92 | 207.2 | 897.91 | 16.064 | 3.13916 | 1850 | 2065.3 | 1475 | 1534.9 | 3.601 | 3.6684 3.7023 |
| 1180 | 1254.34 | 222.2 | 915.57 | 15.241 | 3.15916 | 1900 | 2127.4 | 1655 | 1582.6 | 3.295 | 3.7354 |
| 1200 | 1277.79 | 238.0 | 933.33 | 14.470 | 3.17888 | 1950 | 2189.7 | 1852 | 1630.6 |  |  |
| 1220 | 1301.31 | 254.7 | 951.09 | 13.747 | 3.19834 | 2000 | 2252.1 | 2068 | 1678.7 | 2.776 | 3.7677 3.7994 |
| 1240 | 1324.93 | 272.3 | 968.95 | 13.069 | 3.21751 | 2050 | 2314.6 | 2303 | 1726.8 | 2.555 | 3.8303 |
| 1280 | 1348.55 1372.24 | 290.8 310.4 | 986.90 | 12.435 | 3.23638 | 2100 | 2377.4 | 2559 | 1775.3 | 2.356 | 3.8605 |
|  | 1372.24 | 310.4 | 1004.76 | 11.835 | 3.25510 | 2150 | 2440.3 | 2837 | 1823.8 | 2.175 | 3.8901 |
|  |  |  | - | - | . | 2200 | 2503.2 | 3138 | 1872.4 | 2.012 | 3.9191 |
|  |  |  |  |  |  | 2250 | 2566.4 | 3464 | 1921.3 | 1.864 | 3.9474 |

[^0]


[^0]:    Sokree: Adnpted from K. Wark, Thermodynamies, 4th ed., McGraw-Hill, New York, 1983, as based on J. H. Keenan and J. Kaye, Gas
    Tables. Wiley. New York, 1945.

